

# Kemper County IGCC – Overview and Operational Summary

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### Agenda



- Major components and unique features
- Process block flow diagram
- Operational summary and statistics
- Remaining technical challenges
- Conclusions
- Next steps

### **Timeline and Safety**

- Project groundbreaking
- Construction begins
- Combined-cycle in service
- First coal feed to gasifier
- Operations suspended
- Total project man-hours
- Total plant man-hours

June 2010 First half of 2011 Third quarter 2014 July 2016 June 28, 2017 41+ MM Recordable Incident Rate (RIR) = 0.42~2.5 MM RIR = 0.16



## **Kemper County IGCC Overview**

#### Mine-mouth lignite

#### • 2x1 IGCC

- Two Transport Gasifiers (TRIG™)
- Two Siemens SGT6 5000F CTs
- One Toshiba steam turbine
- 65+% carbon capture
  - ~800  $lb_{CO2}/MWh_{net}\, or\,$  ~550  $lb_{CO2}/MWh_{gross}$
- 582 MW peak and 526 MW on syngas
- Heat rate 12,150 Btu/kWh<sub>NET</sub>

### • Byproducts (TPY)

- ~3,800,000  $CO_2$  used for EOR
- ~150,000 sulfuric acid
- ~19,000 ammonia

Kemper Lignite Composition						
		Average	Min	Max		
Heat Content	btu/lb	5,290	4,765	5,870		
Moisture	%	45.5	42	50		
Ash	%	12.0	8.6	17		
Sulfur	%	1.0	0.35	1.7		





### **Kemper Project Map**

- ~70 miles transmission
- ~60 miles CO<sub>2</sub> pipeline (for EOR)
- ~5 miles natural gas
  pipeline
- ~30 miles treated
  effluent line



#### **Kemper Block Flow Diagram Tested at PSDF** Not Tested at PSDF Patented by Southern (Commercially Available) (Commercially Available) Company **GASIFIER ISLAND** AIR **CFAD** WSA SULFURIC ACID Fine Ash Cooling and ACID Process GAS LIGNITE Depressurization **GASIFIER** Low-Temp Syngas $CO_2$ and High-Temp $CO_2$ Lignite High-SYNGAS Water-Particulate Cooling and Sulfur Drying and Pressure Syngas Gas Shift Collection



### **Operational Summary**



- Achieved fully integrated operation of entire IGCC
  - Both CTs produced power with syngas
  - Steam turbine produced power with superheated steam from the syngas coolers
  - On spec production of byproducts  $CO_2$ , anhydrous ammonia, sulfuric acid
- First-of-a-kind commercial TRIG<sup>™</sup> gasification system
  - Availability as good or better than other gasification technologies during first year operation
  - 90% gasifier availability
- Availability following expected availability ramp
- Kemper operation suspended primarily due to dramatic decrease in price and forecast for natural gas
  - Natural gas prices and forecast decreased 60-70% since 2010 project approval

#### **Coal IGCC Plant Syngas Production Availabilities**









#### **TRIG Advantages**

- No internal burners / fuel injectors
- Longer refractory life
- Dry ash no molten slag or corrosive / erosive blackwater system
- Higher carbon conversion → less tar → less syngas cooler fouling

### **Key Operating Statistics**



- Gasifier operation
  - 224 total days of lignite gasification
  - Achieved 100% gasifier design coal feed capacity
- Syngas cleanup/emissions
  - Met all environmental permit requirements
  - Achieved design 65% CO<sub>2</sub> capture and transport for Enhanced Oil Recovery (EOR)
  - On spec production of CO<sub>2</sub>, ammonia and sulfuric acid
- CT operation on syngas
  - 73% capacity achieved at 170 MW
    - Siemens limited CT capacity on syngas to 70% until June 2017, then increased to 80%
  - 164,900 MWh generated with syngas

#### Inconsistent raw coal quality

- Frequently outside design range for both moisture and particle size
- Modifications in May-June 2017
  improved reliability
- Before modifications, sustained 80% gasifier coal feed capacity with <u>three</u> dryers
- After modifications, sustained 80% gasifier coal feed capacity with <u>two</u> dryers.
- Additional changes were being developed and implemented



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# Refractory replacement in the gasifier seal leg outlet

- Refractory improperly installed in shop experienced significant and uncharacteristic spalling during drying, but construction schedule prevented refractory replacement
- Bottom sections replaced in situ during commissioning and worked well thereafter
- Upper section spalled from the seal leg, blocking ash removal and requiring periodic clean-out
- Refractory replacement scheduled for upcoming October 2017 outage would have eliminated significant spalling



#### Syngas cooler superheater tube leaks

- Numerous leaks developed at tube supports of Coil 5 on multiple superheaters
- Finite element analysis revealed insufficient tube thickness/design margin at tube support weld connections
- All Coil 5 tubes plugged in each train's Superheater II prior to June 2017
  - Sufficient heat transfer area remaining for full coal feed rates because less tube fouling than expected
  - Inner coils likely under less overall stress than Coil 5 per engineering evaluations
- No additional tube failures, but insufficient operating time to prove conclusively reliable





# Excess sour water production from syngas scrubbers

- Damage to scrubber internals and design of chimney trays allowed excessive water bypassing to sour water system
- Sour water system overwhelmed with two gasifier trains at higher coal feed rates
- Chimney tray redesign scheduled for October outage would have resolved this issue



# Salt formation in the Sour Water system

- High sour water pH preventing adequate separation of ammonia, CO<sub>2</sub> and H<sub>2</sub>S
- Ammonium bisulfide salts forming in ammonia purification equipment, limiting capacity and reliability at high coal feed rates
- Acid and caustic injection changes in progress to increase pH control and improve separation





### Conclusions



- Core TRIG<sup>™</sup> technology successfully demonstrated at commercial scale
  - Operated at 100% of coal feed design
  - Produced syngas suitable for power generation in the CT
- Kemper IGCC demonstrated with dual-train operation
  - Modifications required to sustain operation of both trains simultaneously and to achieve the long-term availability ramp
- Fuel price differential between natural gas and lignite was the primary reason for suspension of operations prior to making the identified modifications for sustained dual-train operation

### **Next Steps**



- Evaluate and develop best practices and lessons learned from design, construction, startup and operations of the Kemper IGCC project
- Continue supporting DOE mission to advance clean coal and carbon capture technologies
  - Commissioning report with lessons learned
  - Final Full Project report with lessons learned
  - TRIG<sup>™</sup> reference plant with expected capital and operating costs for nextgeneration TRIG<sup>™</sup> IGCC
- Continue supporting development of clean coal technologies to ensure they are ready to serve energy needs where fuel costs and carbon capture credits make them economically competitive

### **Questions?**



