#### **IEA 4th Post Combustion Capture Conference:**

#### CO<sub>2</sub> Capture by Cold Membrane Operation (DE-FE0013163 & FE0026422)



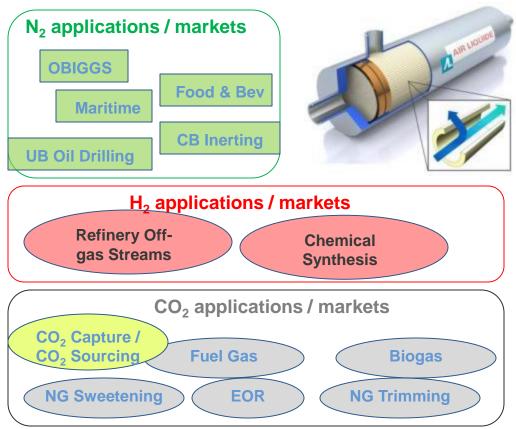
September 5, 2017 A. Augustine, T. Chaubey, S. Kulkarni, D. Hasse, S. Fu, J.M. Gauthier | R&D

#### Air Liquide and MEDAL



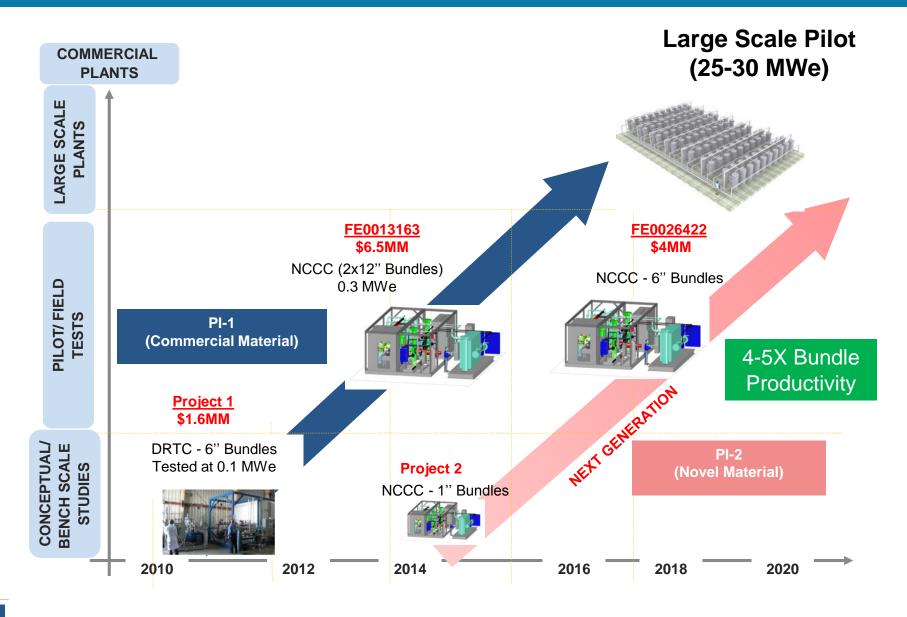


World leader in industrial and medical gases 68,000 employees \$19 billion sales (2016)



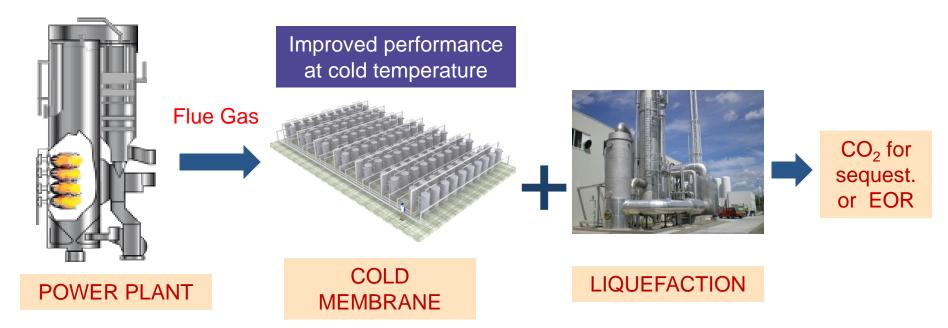


#### Cold Membrane Technology Roadmap



## Technology Summary

Air Liquide hybrid cold membrane / liquefaction process for 550 MWe scale



Cold membrane testing at 0.1 MWe with synthetic flue gas (TRL4) in 2012

CO<sub>2</sub> Capture Cost estimated at 46-52\$/tonne (DOE Target - \$40/tonne)

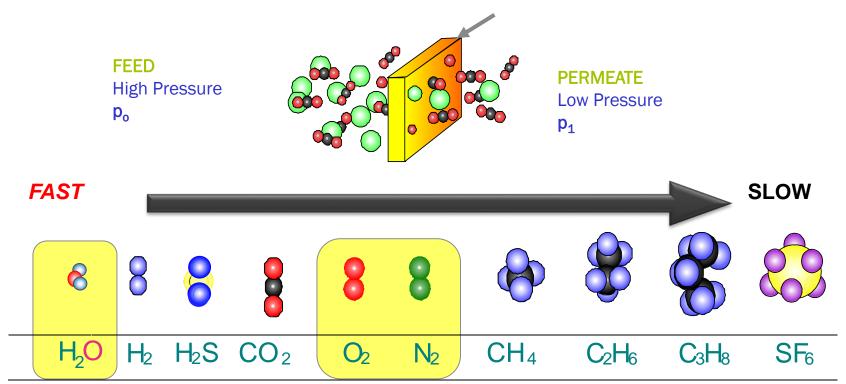
Tested PI-1 material at 0.3 MWe scale (TRL5) at the NCCC

Plan to test novel PI-2 material at 0.3 MWe scale at the NCCC, late 2017



#### Membranes at a Glance

# A thin barrier that allows selective passage of molecules at different rates

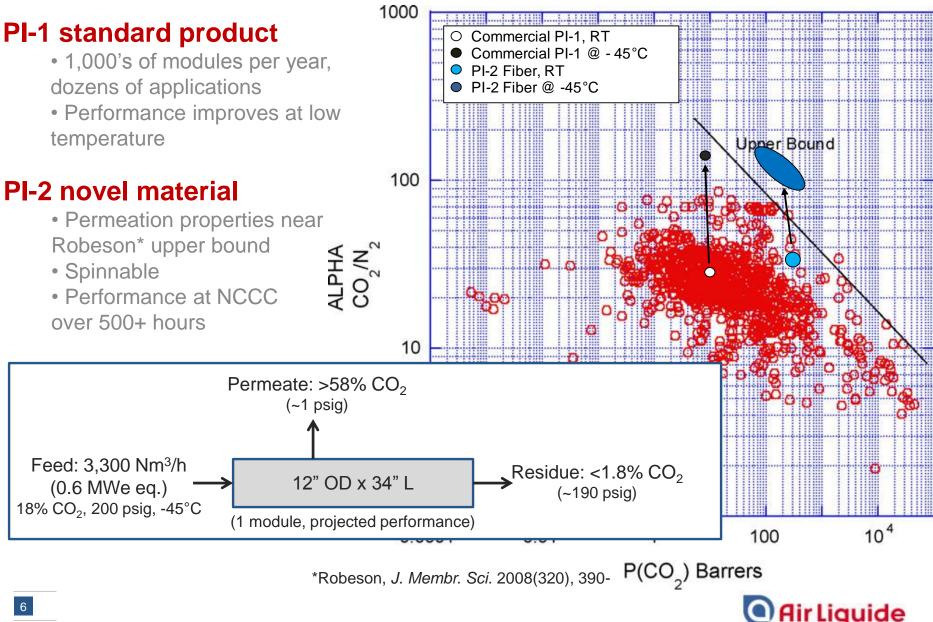


#### A simple technology which requires

- ... no moving parts
- ... no external energy



## **Background: Novel PI-2 Membrane Material**



## Agenda

## Project & Technology Overview

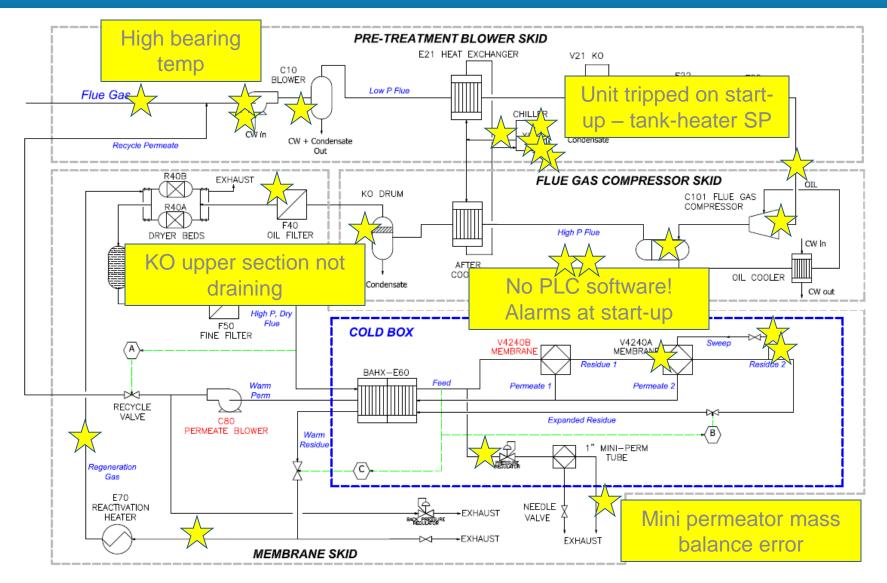
## NCCC Testing

- Installation/Commissioning
- PI-1 commercial membranes
- PI-2 novel material
- 550 MWe TEA
- Next Steps
  - PI-2 manufacturing
    Bench scale performance
    NCCC test plan

(early 3-D mock-up of 0.3 MWe skid)



## Field Test Unit Commissioning at NCCC



Key takeaway: thorough acceptance test and commissioning!



## DRTC TEAM AT NCCC: Install: Aug-2015, Testing: Oct-2015

ENERGY

AIR LIQUIDE

Interna

NETL

INT

5:00000

Sterling

----

## Testing at the NCCC

## PO-4 (Oct – Dec 2015) Objectives:

Validate enhanced performance with real flue gas

Long term test with PI-1 and small (1") PI-2

## **PO-5 (May – Nov 2016)**:

Parametric testing 6" and 12" PI-1 bundle, 1" PI-2

Flue gas contaminants analytical campaign

## **PO-7 (Nov'17 – Dec'17):**

Parametric testing 6" PI-2 bundles

Long term test (500 hours, 90% capture)

## PO-8 (mid-2018?):

Some interesting stuff!



Complete

Complete

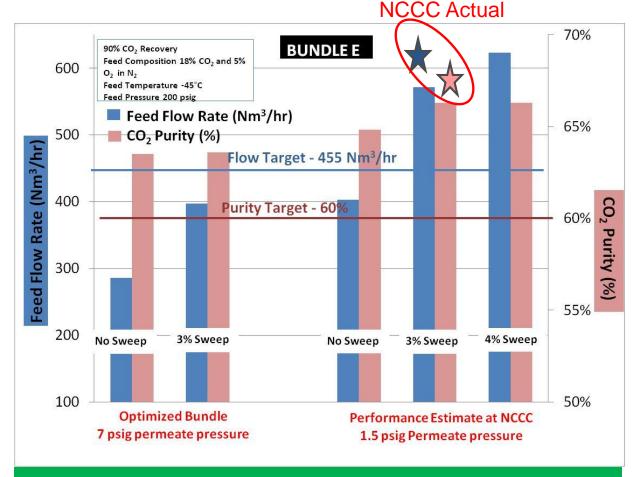
Planned Planned

Planned



## Performance Validation (12" Commercial Bundle)

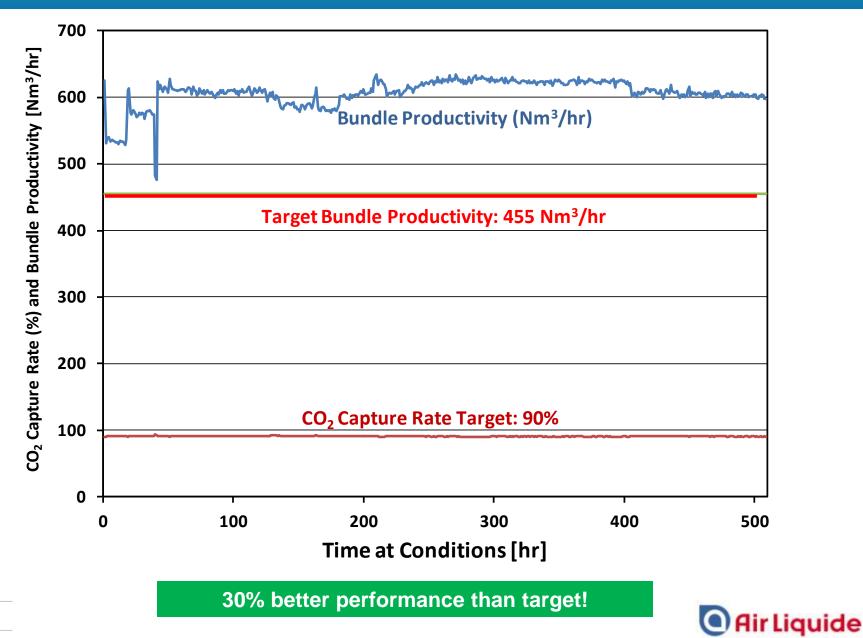
- Bundle performance in field was projected from 0.1 MW bench scale skid
- Actual performance was even better than predicted



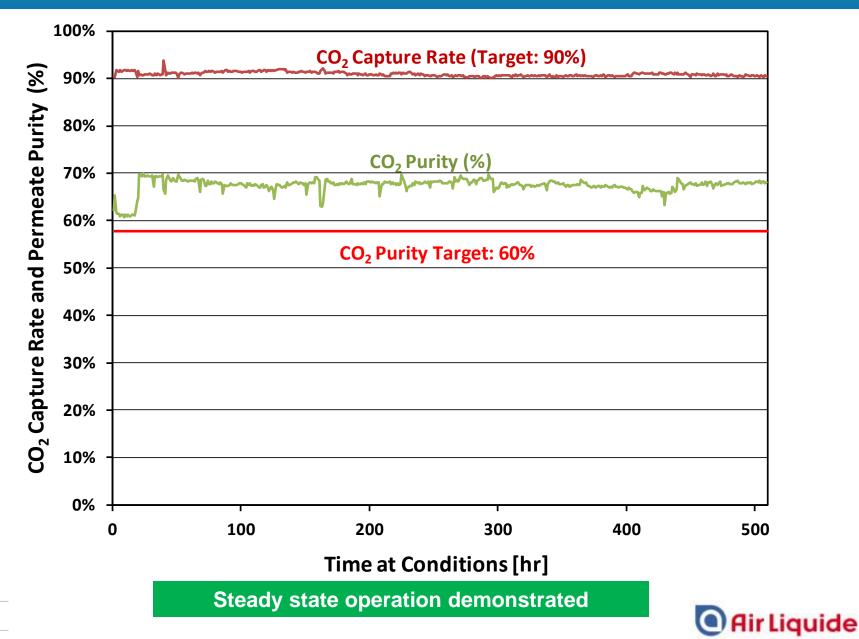
Enhanced membrane performance validated in field!

**Air Liquide** 

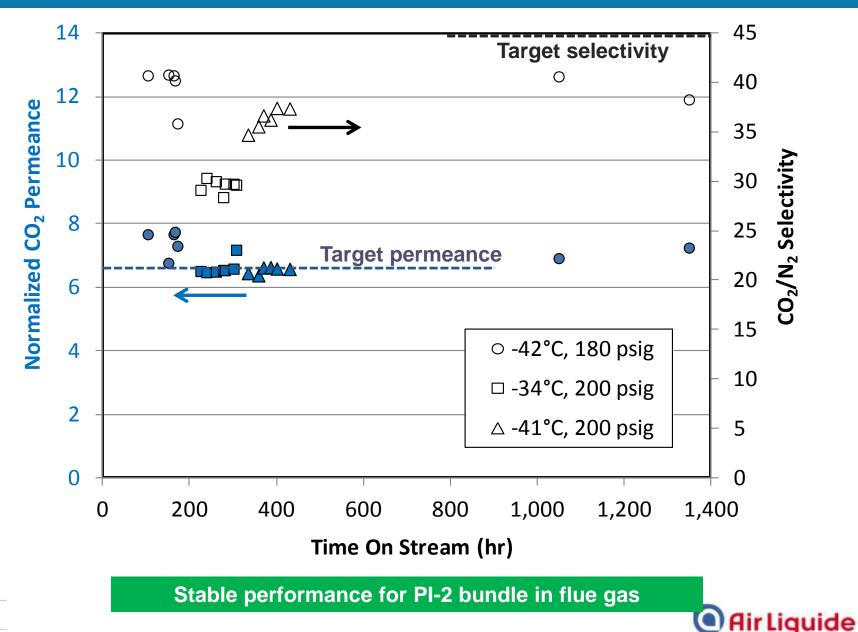
## 12" PI-1 Commercial Bundle Steady State Test



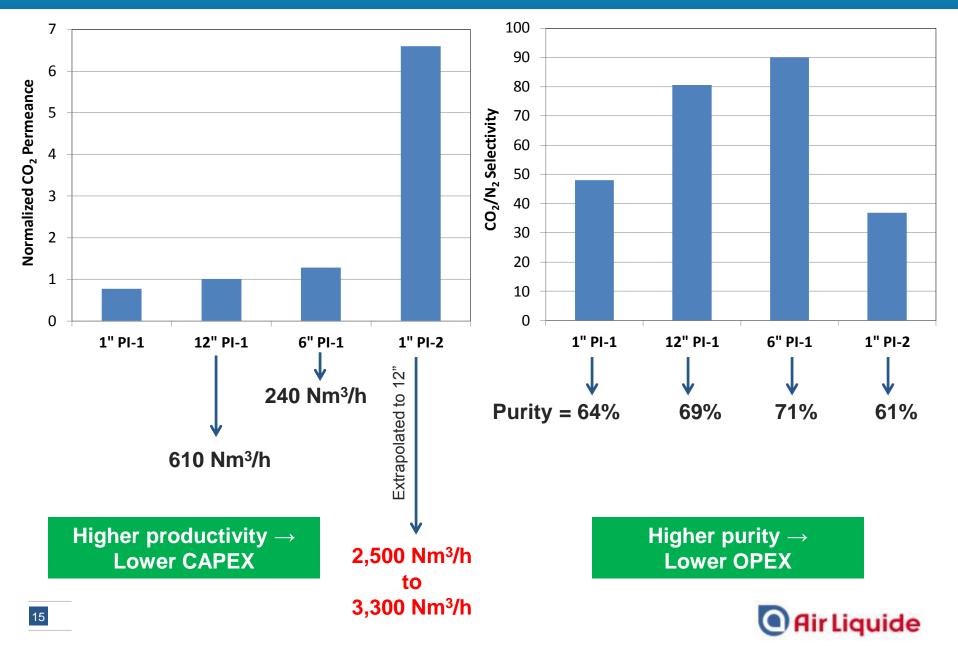
## 12" PI-1 Commercial Bundle Steady State Test



#### PI-2 Steady State Test (1" Bundle: 10x More Fibers)



#### 12" PI-1 vs PI-2 Bundle Performance



## Agenda

## Project & Technology Overview

## NCCC Testing

- Installation/Commissioning
- PI-1 commercial membranes
- PI-2 novel material

## 550 MWe TEA

## Next Steps

PI-2 manufacturing
 Bench scale performance
 NCCC test plan

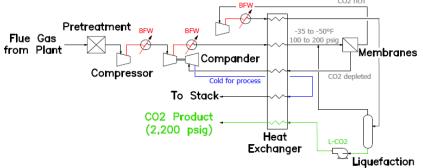
(early 3-D mock-up of 0.3 MWe skid)



## Techno-Economic Analysis (TEA)

# Objective: CO<sub>2</sub> capture from a commercial power plant, 550MWe (net), 12,000 tpd, at \$40/tonne by 2025

Process optimization (PFD → HYSYS model, massenergy balance)



Equipment costing (vendor quotes, scaling method)

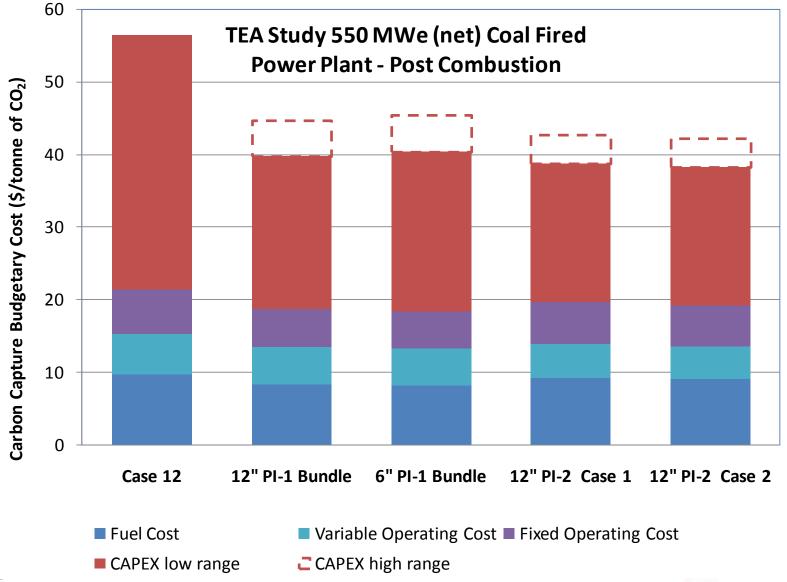
Major Equipment	Scaling Factor	<b>Cost Reference</b>	
Pre-FGD heat recovery	UA value	AL database	
2-stage contact tower	Molar flow	AL database	
Particulate filter	Molar flow	Vendor quote	
Feed compressor	Molar flow	Vendor quote	
Equipment 5, 6, 7, etc.			



DOE cost methodology

Parsons review and feedback

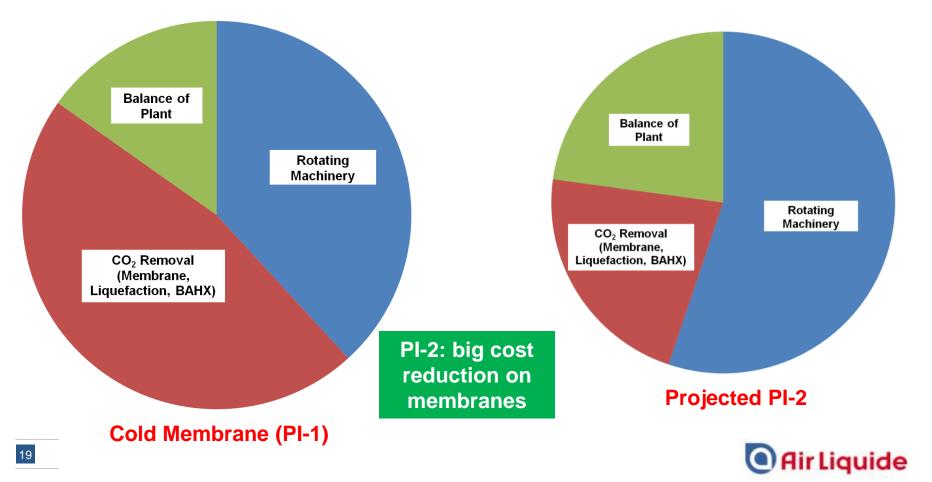
#### Carbon Capture Cost Estimate





## Techno Economic Analysis (TEA) Study

	Case 12 (Amine)	Cold Membrane (PI-1)	PI-2
Power Plant Cost (MM\$)	1,366	1,305	1,326
CO <sub>2</sub> Capture System (MM\$)	593	357	254
Total Plant Cost (MM\$)	1,959	1,662	1,580



### Agenda

## Project & Technology Overview

## NCCC Testing

- Installation/Commissioning
- PI-1 commercial membranes
- PI-2 novel material

## 550 MWe TEA

## Next Steps

PI-2 manufacturing

Bench scale performance

NCCC test plan

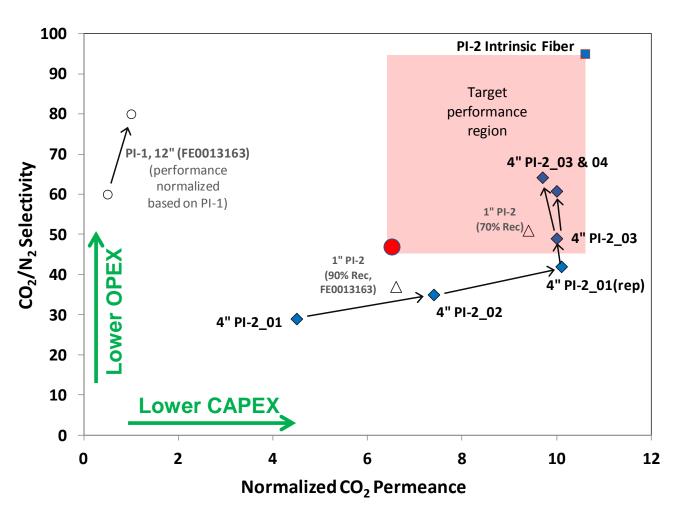
(early 3-D mock-up of 0.3 MWe skid)



## Membrane Manufacturing Scale-up, DE-FE0026422

		OD (in)	Length (ft)	Fiber Count	Spinning Device	Fabrication Technique			
Mini permeator	÷	0.25 - 0.5"	4.07	<1000	1-hole lab unit	Hand			
Permeator	÷	1"	1.6'	1 – 5x		Cleain			
Skein module		2.5"		15 – 20x	12-hole	Skein			
R&D prototype bundle	-	2.5 - 4"		15 – 20x	"DSU"				
6" bundle		6"	2.8'	50 – 90x		Forming			
In	pro	gress, ready	24/36-hole production	r onning					
12" bundle (commercial)		12"		>200x	unit				
Spinning Equipment (DSU) Fiber Processing / Handling Forming Equipment									
Spinning     Post-spin handling       Washing     Drying       Bobbin winding									

#### 4" Prototype Bundle Performance



- Significant improvement by using 'forming' method in scale-up
- Lessons learned resulting in further performance gains
- Epoxy application for tubesheet
- 2) Post-treatment solution concentration
- Outer wrap layer positioning
- 4) Optimize fiber OD

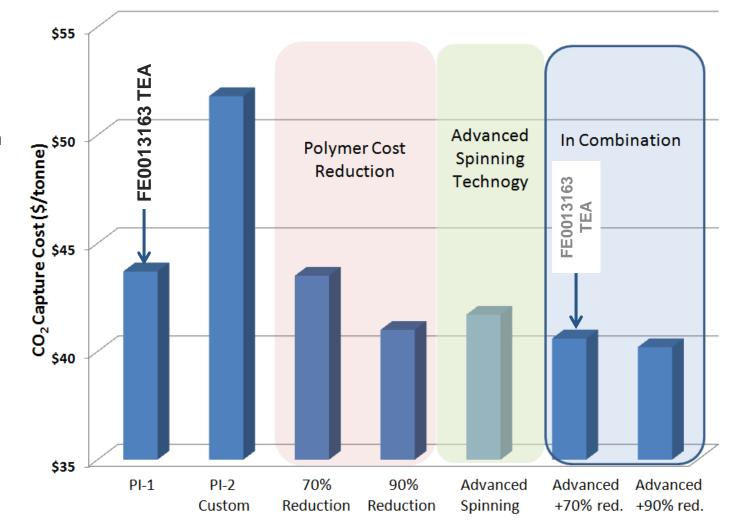
Success criteria: 90 Nm<sup>3</sup>/h feed flow, 90% CO<sub>2</sub> recovery, 58% permeate purity



## Fiber Manufacturing Cost Analysis

#### What are relative merits of costsaving approaches?

- Best value is
   composite formulation
- With low polymer price monolith fiber yields CO<sub>2</sub> capture cost savings
- Pursuing both approaches





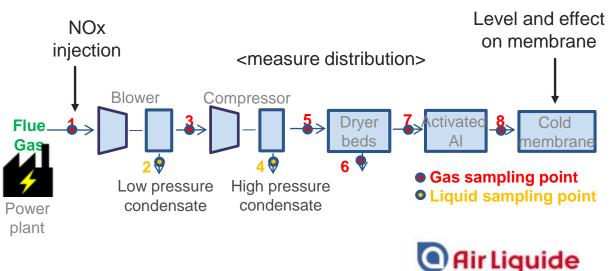
## **Next Steps**

Manufacturing several 6" bundles
(6 – 8), test on 0.1 MWe skid in
Newark, DE

- Field-test at NCCC, 0.3 MWe scale
  - Parametric testing
  - Long-term stability
  - Dynamic testing: start / stop / cool / warm / moisture breakthrough – evaluate bundle integrity
  - NO/NO<sub>2</sub> injection to simulate SCR failure/removal



0.3 MWe Field-Test Unit at NCCC, Pilot Bay 3 (DE-FE0013163)



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- Parsons Government Services

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